Buoyancy-driven flow in a confined aquifer with a vertical gradient of permeability

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We examine the injection of fluid of one viscosity and density into a horizontal permeable aquifer initially saturated with a second fluid of different viscosity and density. The novel feature of the analysis is that we allow the permeability to vary vertically across the aquifer. This leads to recognition that the interface may evolve either as a rarefaction wave which spreads at a rate proportional to t, a shock-like front of fixed length, or a mixture of shock-like regions and rarefaction wave type regions. The classical solutions in which there is no viscosity ratio between the fluids and in which the formation has constant permeability lead to an interface which spreads laterally at a rate proportional to $t^{1/2}$. However, these solutions are unstable to cross-layer variations in the permeability owing to the vertical shear which develops in the flow, causing the structure of the interface to evolve to the rarefaction wave or shock-like structure. In the case that the viscosities of the two fluids are different, it is possible that the solution involves a mixture of shock-like and rarefaction type structures as a function of the distance above the lower boundary. Using the theory of characteristics we develop a regime diagram to delineate the different situations. We consider the implications of such heterogeneity for the prediction of front locations during CO_2 sequestration. If we neglect the permeability fluctuations the model always predicts rarefaction type solutions, while even modest changes in the permeability across a layer can introduce shocks. This difference may be very significant since it leads to the CO_2 plume occupying a greater fraction of the pore space between the injector and the leading edge of the CO_2 front in a layer of the same mean permeability. This has important implications for estimates of the fraction of the pore space which the CO_2 may access.

Key words:

1. Introduction

Buoyancy driven flow in permeable rock has been the focus of a considerable research effort given the importance of such effects for many environmental and energy related processes, including enhanced oil recovery and carbon sequestration (Lake 1989; Huppert & Woods 1995; Riaz *et al.* 2006; Huppert & Neufeld 2014; Woods 2014). Analyses have been carried out for relatively thin and hence confined aquifers and much deeper unconfined reservoirs, and the adjustment from an effectively unconfined flow at short times, to a confined flow at long times was explored by Zheng *et al.* (2015). The effects of a non-uniform viscosity ratio leads to the development of rarefaction waves and shocks (Lajeunesse *et al.* 1999; Juanes *et al.* 2010; Gunn & Woods 2011) while the effects of

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the gradual dissolution of the CO_2 and capillary trapping of the CO_2 have been shown to cause the currents to gradually wane (Pruess *et al.* 2004; Hesse *et al.* 2006). The role of capillary pressures impeding the advance of CO_2 through seal rock has also been explored (Woods & Farcas 2009) as well as the case in which fluid leaks off the current (Pritchard *et al.* 2001). Models have also been developed to account for two phase flow effects (Golding *et al.* 2011).

The majority of these models have assumed that the formation is of uniform permeability. This leads to the simplifying result that the speed of the current is uniform with depth. However, in real geological strata, there are often multiple layers of different permeability. Reservoirs are typically made up of sedimentary rock which is very inhomogeneous and the contrasts in permeability can totally dominate fluid flow (Bjorlykke 1993). Also within single geological flow units, such as are produced from massive turbidites flows on the sea-floor, the grain size is expected to gradually change with depth in the deposit as the parent turbulent flow either waxes or wanes.

While some of the effects of layering which can lead to the dispersion of buoyant plumes and gravity currents in a geological strata have been examined (Fayers *et al.* 1992; Hesse & Woods 2010; Guo *et al.* 2016*a*; Farcas & Woods 2016), there is much less analysis of the effects of permeability gradients across an individual flow unit.

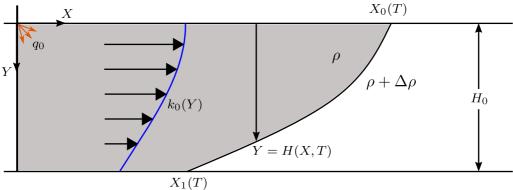
The purpose of this paper is to explore how a linear increase or decrease of permeability with height in a permeable layer influences the buoyancy driven flow through that layer. The critical physical effect which this introduces is the variation of flow speed with vertical position in the layer, and we show that this can lead to some fundamentally different controls on the flow compared to a homogeneous reservoir.

In section 2, we introduce a model for a gravity driven flow in a confined permeable rock in which the permeability varies with height. We then present some numerical solutions of the resulting non-linear advection-diffusion equation for the evolution of the interface between the injected fluid and the original fluid in the system. This identifies that, under different conditions, there are rarefaction wave type solutions, travelling wave type solutions, and mixtures of these solutions at different depths in the layer. We then compare long-time asymptotic rarefaction wave and travelling wave solutions of the governing equation with the full numerical solutions. We discuss the implications of these results, in comparison with the very different current structure that develops in a homogeneous porous layer, when each fluid has the same viscosity, in which the front of the flow spreads at a rate proportional to $t^{1/2}$. In section 4 we develop a short time asymptotic analysis of the governing equation, following the approach of Zheng *et al.* (2015). We analyse how a permeability gradient and viscosity ratio affect the early time behaviour which asymptotes to that of an unconfined gravity current.

We conclude with a discussion focussing on the challenges of predicting the storage capacity of an aquifer by illustrating how the fraction of the pore space which may be flooded with CO_2 varies if we account for cross-layer variations in permeability and illustrating that with more complex vertical structure for the permeability, it is possible to have multiple shock regions separated by rarefaction wave regions.

2. Model

We assume liquid of density ρ and visocity μ_i is injected into a horizontal, laterally extensive aquifer initially filled with liquid of density $\rho + \Delta \rho$ and viscosity μ_a (figure 1). The aquifer has depth H_0 , porosity ϕ and fluid is injected at X = 0, Y = 0 with a flow rate q_0 . The vertically varying permeability $k_0(Y)$, is independent of horizontal position. In the region where the aquifer is fully flooded by the injected fluid, the flow



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Figure 1: Schematic diagram showing the model problem for constant injection into a vertically heterogeneous aquifer.

will be pressure driven, whilst in the slumping region between the two contact points, flow will be driven by a mixture of buoyancy and the background pressure gradient. We assume the fluids are incompressible, the motion is governed by Darcy's law and that there is a sharp interface between the immiscible fluids. Once the invading fluid has spread beyond a distance $L \gg H_0$ from the well, the pressure becomes approximately hydrostatic (Bear 1971; Huppert & Woods 1995) and is given by

$$P(X, Y, T) = \begin{cases} P_0 + \rho g Y & 0 < Y < H \\ P_0 + (\rho + \Delta \rho) g Y - \Delta \rho g H & H < Y < H_0 \end{cases}$$
(2.1)

where $P_0 = P(X, 0, T)$ is the unknown pressure at the top of the aquifer. Using Darcy's law for the horizontal component of the flow,

$$u_{i} = -\frac{k_{0}(Y)}{\mu_{i}}\frac{\partial P_{0}}{\partial X}, \quad u_{a} = -\frac{k_{0}(Y)}{\mu_{a}}\left(\frac{\partial P_{0}}{\partial X} - \Delta\rho g\frac{\partial H}{\partial X}\right)$$
(2.2)

where u_i , u_a are the transport velocities of the injectate and ambient fluid, respectively. Local mass conservation for the injected and ambient fluids may be expressed in the form,

$$\phi \frac{\partial H}{\partial T} = -\frac{\partial}{\partial X} \left(\int_0^H u_i \mathrm{d}Y \right), \quad \phi \frac{\partial (H_0 - H)}{\partial T} = -\frac{\partial}{\partial X} \left(\int_H^{H_0} u_a \mathrm{d}Y \right). \tag{2.3}$$

Adding these two equations together provides an equation for the conservation of mass of the current,

$$\int_{0}^{H} u_{i} \mathrm{d}Y + \int_{H}^{H_{0}} u_{a} \mathrm{d}Y = q_{0}.$$
(2.4)

This can be recast as a constraint for the global mass conservation of the injected fluid,

$$\phi \int_0^{X_0(t)} H(X,T) \mathrm{d}X = q_0 T, \tag{2.5}$$

where $X_0(T)$ is the contact point along the top of the aquifer (see figure 1), and we have assumed injection begins at T = 0. We use the aquifer height H_0 and the verticallyaveraged permeability,

$$\bar{k} = \frac{1}{H_0} \int_0^{H_0} k_0(Y) \mathrm{d}Y$$
(2.6)

to introduce the dimensionless quantity,

$$K_0(H) = \frac{1}{H_0 \bar{k}} \int_0^H k_0(Y) \mathrm{d}Y.$$
 (2.7)

Note that $K_0(0) = 0$, $K_0(H_0) = 1$, and in a uniform aquifer, $K_0(H) = H/H_0$. The unknown pressure, P_0 can be eliminated by substituting the expressions for the Darcy velocities (2.2) into equation (2.4). Local mass conservation for the injectate (2.3a) then leads to the advection-diffusion type equation for the depth of the current,

$$\phi \frac{\partial H}{\partial T} + q_0 \frac{\partial}{\partial X} \left(\frac{K_0(H)}{K_0(H) + M(1 - K_0(H))} \right) = U H_0 \frac{\partial}{\partial X} \left(\frac{M K_0(H)(1 - K_0(H))}{K_0(H) + M(1 - K_0(H))} \frac{\partial H}{\partial X} \right),$$
(2.8)

where

$$U = \frac{\Delta \rho g \bar{k}}{\mu_i}, \quad M = \frac{\mu_i}{\mu_a} \tag{2.9}$$

are the velocity associated with the buoyant slumping of the injectate, and the viscosity ratio, respectively. To complete the mathematical description, we require initial and boundary conditions. Injection begins at T = 0 so

$$H(X,0) = 0. (2.10)$$

At the contact point along the top of the aquifer, $X = X_0(T)$, the boundary condition is

$$H(X_0(T), T) = 0. (2.11)$$

Differentiating the equation for mass conservation (2.5) with respect to time and applying the boundary condition (2.11) gives

$$\phi \int_0^{X_0(t)} \frac{\partial H}{\partial T} \mathrm{d}X = q_0. \tag{2.12}$$

By integrating (2.8) between X = 0 and $X = X_0(T)$, and applying (2.11) and (2.12) we obtain the boundary condition at X = 0;

$$\left[q_0 \frac{K_0(H)}{K_0(H) + M(1 - K_0(H))} - UH_0 \frac{MK_0(H)(1 - K_0(H))}{K_0(H) + M(1 - K_0(H))} \frac{\partial H}{\partial X}\right]\Big|_{X=0} = q_0. \quad (2.13)$$

Note that the governing equation (2.8) and the boundary conditions (2.11), (2.13) do not change when the aquifer becomes fully flooded by the injectate.

2.1. Non-dimensionalization

Balancing the contributions from the net flow and the buoyant slumping in the nose region of the current, leads to the scalings

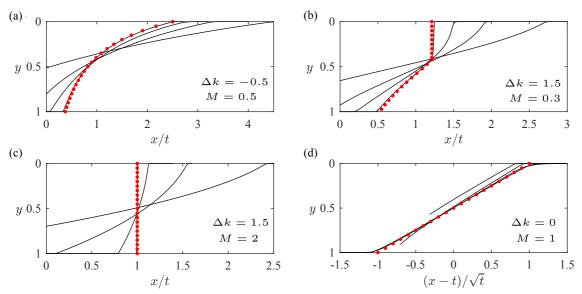
$$h = \frac{H}{H_0}, \quad y = \frac{Y}{H_0}, \quad x = \frac{q_0}{UH_0^2}X, \quad t = \frac{q_0^2}{\phi UH_0^3}T.$$
 (2.14)

Using these scalings and the functions

$$k(y) = \frac{k_0(Y)}{\bar{k}}, \quad K(y) = K_0(Y),$$
(2.15)

we can re-express equation (2.8) in dimensionless form,

$$\frac{\partial h}{\partial t} + \frac{\partial}{\partial x} \left(\frac{K(h)}{K(h) + M(1 - K(h))} \right) = \frac{\partial}{\partial x} \left(\frac{MK(h)(1 - K(h))}{K(h) + M(1 - K(h))} \frac{\partial h}{\partial x} \right).$$
(2.16)



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Figure 2: Numerical simulations of the injection of buoyant fluid into a stratified porous medium from early to late times. The interface is shown at t = 0.1, 0.5, 2.5 and 62.5 in similarity coordinates for four different sets of parameter values (a-d). The late-time asymptotic solutions found in section 5 are shown as red dots and they agree well with the t = 62.5 numerical solution. (a) shows a rarefaction wave, asymptotic shape given by equation (5.7), (b) is a compound interface with shock and rarefaction regions, the shape of the shock is given by equation (5.19), (c) is a full shock, shape given by equation (5.11), and (d) is the case of uniform permeability and equal viscosities which leads to a front that grows in proportion to $t^{1/2}$, the shape was found by Huppert & Woods (1995). These four panels characterise the four possible late time regimes, shown in parameter space in figure 4.

Our choice of scalings (2.14) has removed the buoyancy parameter,

$$B = \frac{q_0}{UH_0},\tag{2.17}$$

from the governing equation so that, in dimensionless terms, buoyancy dominates in $t \ll 1$ and the net flow driven by pressure in $t \gg 1$. The initial condition is h(x,0) = 0. The boundary condition at the leading contact point, $x = x_0(t)$, is $h(x_0(t), t) = 0$. The dimensionless form of the X = 0 boundary condition (2.13) is,

$$\left\lfloor \frac{K(h)}{K(h) + M(1 - K(h))} - \frac{MK(h)(1 - K(h))}{K(h) + M(1 - K(h))} \frac{\partial h}{\partial x} \right\rfloor \bigg|_{x=0} = 1.$$
(2.18)

At early times, when the aquifer has not been fully flooded by the injectate and h(0,t) < 1, the boundary condition (2.18) can be rearranged. First, we multiply by K(h) + M(1 - K(h)), the K(h) terms then cancel, and dividing by M(1 - K(h)) gives,

$$1 = \left[-K(h)\frac{\partial h}{\partial x} \right] \bigg|_{x=0}.$$
 (2.19)

At later times h(0, t) = 1 and such a rearrangement is not possible because the last step was dividing by M(1 - K(h)). Instead, we observe that h = 1 satisfies equation (2.18) for any value of $\partial h/\partial x$. The flooding of the aquifer implies a second contact point at the base of the aquifer with $h(x_1(t), t) = 1$, where $x_1(t) < x_0(t)$ (see figure 1).

3. Numerical simulation

We conducted direct numerical simulations of the nonlinear advection-diffusion equation (2.16) with appropriate boundary conditions following the approach of Zheng *et al.* (2015) using the finite difference scheme of Kurganov & Tadmor (2000). Whilst the model in section 2 applies for any k(y), we first choose to use a linear stratification,

$$k(y) = 1 + \Delta k \left(y - \frac{1}{2} \right).$$
 (3.1)

Here $\Delta k = k(1) - k(0)$, is the dimensionless permeability difference between the top and the base of the aquifer, and has values in the range $-2 < \Delta k < 2$.

Figure 2 shows the numerical results at early and late times, illustrating how the interface transitions to the late time solution (red dots). The long time solutions are independent of the vertical location of the injection well at x = 0 because the injectate has flooded the aquifer. However, at early times the injection height is critical. For our model, we have assumed the injection well is located at x = 0, y = 0. In the early time period, when the current is thin and the interface has not made contact with the lower boundary, we expect that the governing equation (2.16) can be simplified and that the flow resembles that in an unconfined aquifer. This is studied in section 4 in which we develop early time asymptotic solutions and compare these with our numerical simulations (see figure 3). If the fluid was injected at y = 1 the initial flow would form a buoyant plume, leading to a different adjustment towards the gravity-driven flow (see Lyu & Woods 2016). The plume head would develop irregular fingers as it advances towards the top boundary of the aquifer. The injectate subsequently fills the depth of the aquifer in the region near the source and the evolution transitions to the fully-flooded late time regimes described in section 5.

The panels in figure 2 illustrate the four late time regimes for the interface. (a) is a growing rarefaction wave across the whole aquifer which may be identified since the horizontal coordinate is x/t. (b) shows a compound interface consisting of a vertical interface in the upper region which travels at a constant speed V and a growing rarefaction wave in the lower region. In (c), the shock extends across the entire aquifer and travels with unit velocity. (d) is the special case of uniform permeability and unit viscosity ratio for which the interface grows proportional to $t^{1/2}$ as found by Pegler *et al.* (2014) and Zheng *et al.* (2015). These numerical results motivate the late time asymptotic analysis of the four regimes in section 5 which suggests parameter values for which each regime occurs (see figure 4).

4. Early time asymptotic solutions

In this section, we show that the early time evolution is controlled primarily by the permeability at the top of the aquifer and the viscosity ratio. The early regime is valid until $t = \mathcal{O}(0.1)$, which corresponds to the first few weeks of injection in a typical CO₂ storage project (see section 7).

At early times, with the injection well located at the origin, the fluid-fluid interface does not touch the lower boundary of the aquifer and h is small everywhere. The injectate

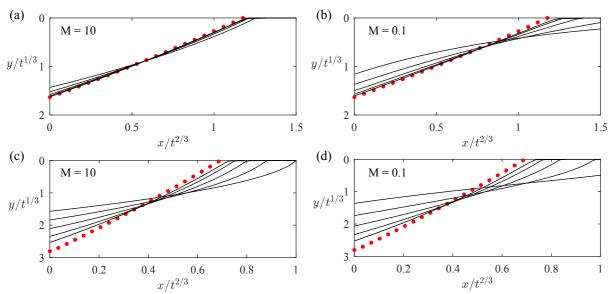


Figure 3: Early evolution of the interface at five times: $t = 10^{-5}$ to $t = 10^{-1}$. The similarity solution found in section 4 is shown in red dots. (a) and (b) are the results for $\Delta k = 1$ and M = 10 and 0.1 demonstrating how the early time period is controlled by M. (c) and (d) are the results for $\Delta k = 1.8$ and M = 10 and 0.1, showing similar divergence rates because when $M \ge k(0)$, the early time period is independent of M.

forms a thin layer at the top of the aquifer and the flow initially resembles an unconfined gravity driven flow (cf. Huppert & Woods 1995). The ratio of the buoyancy force to the pressure associated with the net flow is large at early times and hence the advection term can be neglected. Linearising in K(h), the full governing equation (2.16) may be approximated by the equation:

$$\frac{\partial h}{\partial t} = k(0) \frac{\partial}{\partial x} \left(h \frac{\partial h}{\partial x} \right). \tag{4.1}$$

The early time solution is independent of the viscosity ratio since in this limit, the displacement of the original fluid in the aquifer is not rate limiting. The only parameter in equation (4.1) is k(0). We anticipate that the value of the permeability at only y = 0 is sufficient to describe the early-time regime.

The diffusion equation (4.1) has been well studied by Barenblatt (1952), Hesse *et al.* (2007) and MacMinn *et al.* (2012). For injection with a constant flux, it admits a similarity solution with similarity coordinate $\eta = x/(\sqrt{3k(0)}t^{2/3})$. The leading contact point at the top of the aquifer propagates as $x_0 = \eta_0 \sqrt{3k(0)}t^{2/3}$ where η_0 is to be determined. If we rescale the system, then $s = x/x_0 = \eta/\eta_0$ so that the contact point is at s = 1 and the depth of the current can be written as

$$h = \eta_0^2 t^{1/3} \psi(s). \tag{4.2}$$

Here ψ is the shape function which satisfies:

$$\psi - 2s \frac{\mathrm{d}\psi}{\mathrm{d}s} = \frac{\mathrm{d}}{\mathrm{d}s} \left(\psi \frac{\mathrm{d}\psi}{\mathrm{d}s} \right)$$

$$\psi(1) = 0.$$
(4.3)

Global mass conservation identifies that the contact point is given by

$$\eta_0 = \left(\sqrt{3k(0)} \int_0^1 \psi(s) \mathrm{d}s\right)^{-1/3}.$$
(4.4)

To solve the ODE (4.3) numerically, a second boundary condition is required. Letting $s \to 1^-$ gives $\psi(s) \approx 2(1-s)$, providing the boundary conditions used in the numerical procedure: $\psi'(1-\epsilon) \approx 2$, $\psi(1-\epsilon) \approx 2\epsilon$ where $\epsilon \ll 1$. Solving for ψ gives $h(0,t) = 1.298(t/k(0))^{1/3}$. The numerical solutions to (4.3) are shown in figure 3.

The solutions are valid provided both $h \ll 1$ and $M \frac{\partial h}{\partial x} \gg 1$ (so that buoyancy dominates). The first condition is equivalent to $t \ll k(0)$, whilst the second requires $t \ll \frac{M^3}{k(0)^2}$. If $M = \mathcal{O}(k(0))$ then these times are similar. For $M \gg k(0)$, the early time period is controlled by the first condition and for $M \ll k(0)$, it is controlled by the second (see figure 3). When the aquifer has a much higher permeability at the top than the bottom (i.e. k(0) larger), the early time solution is valid for longer because the injectate can easily migrate along the top of the aquifer driven by the buoyancy and the influence of the pressure gradient associated with the net flow is less significant in this high permeability region (figure 3a and 3b). Conversely, for a channel with low permeability at the top, the buoyancy forces are less effective at shearing out the flow, and the pressure gradient associated with the net flow is less studies have shown that the length of the early time period increases strongly with M up to $M \sim 1$ in a uniform aquifer (MacMinn & Juanes 2009), and our contribution demonstrates that this relationship is valid until $M \sim k(0)$ for aquifers with a linear permeability gradient.

After the initial transient in which equation (4.2) is valid, there is an adjustment regime as the depth of the current increases until it fully floods the aquifer, and the long-time asymptotics apply as explored in section 5.

5. Late time asymptotic solutions

At long times, the permeability profile across the aquifer has a significant influence on the interface evolution, in contrast to the early time evolution. We anticipate that the lateral extent of the current is very large compared to the depth of the layer. This implies that the ratio of the buoyancy force to the pressure associated with the net flow is small. In dimensional terms, this is equivalent to

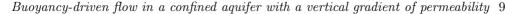
$$\frac{MH_0}{L} \ll 1, \tag{5.1}$$

where L is the length of the interface. The diffusive term on the right hand side of (2.16) can then be neglected. We therefore seek solutions to the equation,

$$\frac{\partial h}{\partial t} + \frac{\partial}{\partial x} \left(\frac{K(h)}{K(h) + M(1 - K(h))} \right) = 0, \tag{5.2}$$

with boundary conditions $h(x_0(t), t) = 0$ and h(0, t) = 1 since the aquifer is fully flooded. This is a scalar first-order linear equation with flux function (see Section 4 of Juanes *et al.* 2010),

$$F(h) = \frac{K(h)}{K(h) + M(1 - K(h))}.$$
(5.3)



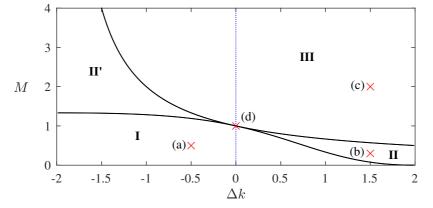


Figure 4: Parameter space for late time solution for linear k(y). For parameter values in region I, given by equation (5.6), the interface tends to a rarefaction wave (figure 2a). In region III, given by equation (5.9), the interface develops a shock across the entire aquifer (figure 2c). For regions II and II', there is a mixed solution (figure 2b). The blue dashed line along $\Delta k = 0$ is the region of parameter space previously studied by Pegler *et al.* (2014) and Zheng *et al.* (2015); the solution at $\Delta k = 0$, M = 1 (see figure 2d) where the interface grows proportional to $t^{1/2}$ is shown to be singular by this figure. Moreover, by including heterogeneous permeability, we have found new compound solutions in II and II' which do not occur along the blue dashed line. The labelled red crosses correspond to the parameter values for the interface shapes in the panels (a-d) in figure 2.

The characteristics are

$$\frac{\mathrm{d}x}{\mathrm{d}t} = F'(h_0(s)) = \frac{Mk(h_0(s))}{[K(h_0(s)) + M(1 - K(h_0(s)))]^2}$$
(5.4)

where $h = h_0(s)$ is the general initial condition on the line x = s, t = 0 in the (x,t) plane and $h_0(s)$ is a decreasing function. The initial conditions either develop into a shock or a rarefaction wave.

5.1. Rarefaction interface

If F'(h) is monotonically decreasing in (0, 1) then the Jacobian is nowhere zero and the method of characteristics can be applied to solve equation (5.2). For the linear k(y) given by equation (3.1), we wish to find values of the parameters, Δk and M for which this solution method is possible and the interface is a rarefaction. The condition that F'(h) is monotonically decreasing across the channel is equivalent to requiring

$$F''(h) \equiv \frac{M\Delta k[K(h) + M(1 - K(h))] - 2M(1 - M)k(h)^2}{[K(h) + M(1 - K(h))]^3}$$
(5.5)

to be negative in all of (0, 1). The denominator is always positive across the channel and the numerator is a quadratic in h since k(h) is linear. The condition for the rarefaction solution can now be found in terms of the parameters,

$$M \leqslant \frac{(\Delta k - 2)^2}{\Delta k^2 - 2\Delta k + 4}.$$
(5.6)



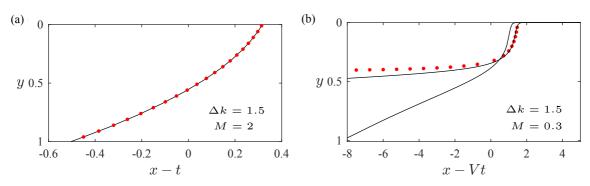


Figure 5: Shocks in travelling wave coordinates. The solid lines are the numerical results and the red dots show the shape predicted by the steady travelling wave solutions found in section 5.2 and 5.3. (a) is the full shock from figure 2c shown at t = 10, it has excellent agreement with the asymptotic shape. (b) is the partial shock from figure 2b shown at t = 10 and t = 100 in coordinates moving at the speed of the shock, given by equation (5.18). Convergence to the asymptotic shape is much slower for the partial shock.

Equation (5.2) then has self-similar solutions $h(x,t) = h(\xi)$, in terms of the similarity variable $\xi = x/t$. The solution is implicitly given by

$$\xi = \frac{x}{t} = F'(h), \tag{5.7}$$

and the contact points satisfy,

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$$x_0(t) = \frac{\left(1 - \frac{\Delta k}{2}\right)t}{M}, \quad x_1(t) = M\left(1 + \frac{\Delta k}{2}\right)t,$$
 (5.8)

at h = 0 and h = 1 respectively. Provided the inequality (5.6) is satisfied, h is a decreasing function of x and the extent of the interface grows in proportion to time implying that the diffusive term in the governing equation (2.16) is $\mathcal{O}(t^{-2})$ whilst the advection term is $\mathcal{O}(t^{-1})$. The interface gradient is $\mathcal{O}(t^{-1})$ and the assumptions made in arriving at equation (5.2) are self-consistent. This analysis is confirmed by comparing the asymptotic solution (5.7), with numerical simulations of the full governing equation in figure 2a.

Figure 4 shows the region (I) in parameter space given by (5.6). If the injectate is sufficiently mobile compared to the ambient fluid $(M \ll 1)$ then the current will run along a thin layer at the top, even if the permeability is much lower there (i.e. $\Delta k \approx 2$). Conversely, when Δk is close to -2 the resistance to flow is so much higher at the bottom of the aquifer that even an injectate which is slightly more viscous than the ambient fluid will spread out along the top as a rarefaction wave. For values of Δk between these two limits, there is a balance between the resistance associated with the low permeability and the resistance associated with the high viscosity. Indeed, the boundary given by the inequality (5.6) has M as a decreasing function of Δk .

5.2. Full shock interface

When the parameter values do not satisfy the inequality (5.6), a shock needs to be introduced to solve equation (5.2). If F'(h) is monotonically increasing in (0,1) then all the characteristics of the advection equation (5.2), given by (5.4), cross and a weak solution (with a discontinuity) can be sought; the solution develops a shock that extends across the whole aquifer from h = 0 to h = 1. The shock requires F''(h) (equation 5.5) to

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be positive in (0, 1). For the linear variation of permeability (equation 3.1), the condition for the full shock in terms of the parameters is,

$$M \geqslant \frac{1}{1 + \Delta k/2}.\tag{5.9}$$

In the absence of gravity, this shock would not occur, instead the buoyant injectate would be driven along the base of the aquifer by the combination of higher permeability and the low viscosity of the ambient fluid. Buoyancy forces balance this effect and so the light injectate rises to the top of the aquifer and the interface travels with constant shape and velocity. Mass conservation implies the shock travels with unit velocity (see figure 2c).

The numerical results in travelling coordinates, shown in figure 5a, can be used to inspect the approximately vertical interface in figure 2b. The shock is not in fact a zerowidth vertical line; it is smoothed by the buoyancy force. We seek to find the shape of this non-vertical shock.

For parameter values such that the full shock condition given by (5.9) is satisfied, the interface moves with unit velocity and this motivates our seeking a travelling wave solution to the full equation (2.16), with $h(x,t) = h(\eta)$ where $\eta = x - t$. Dropping the time derivative and integrating, we find that the shape satisfies,

$$h = 1 \qquad \qquad \eta \leqslant \eta_1 \tag{5.10}$$

$$\frac{\mathrm{d}h}{\mathrm{d}\eta} = \frac{K(h) - Mh + (M-1)hK(h)}{MK(h)(1 - K(h))} \qquad \eta_1 < \eta < \eta_0 \tag{5.11}$$

$$h = 0 \qquad \qquad \eta \ge \eta_0. \tag{5.12}$$

The constant of integration is set to zero because the gradient is finite as $h \to 0$. The contact points are constants, $\eta_0 = x_0(t) - t$, and, $\eta_1 = x_1(t) - t$, at the top and base of the aquifer respectively. Note that $\eta_1 < 0$ and $\eta_0 > 0$. The separation of the contact points can be found by numerically integrating equation (5.11) across the aquifer,

$$\eta_0 - \eta_1 = \int_{h=1}^{h=0} \left(\frac{\mathrm{d}h}{\mathrm{d}\eta}\right)^{-1} \mathrm{d}h.$$
 (5.13)

The shape of the travelling wave interface is independent of the position of the contact points because the right-hand side of equation (5.11) is independent of η . Therefore, we can find the shape by making a arbitrary choice of η_1 . We must then translate this shape in the η direction, corresponding to a correct choice of the contact points. We use mass conservation which is,

$$\eta_1 + A = 0, \tag{5.14}$$

where A is the area under the interface shape in the partially flooded region. We can now find η_1 and η_0 .

The red dots in figure 5a show the travelling wave solution we have just calculated. There is good agreement with the numerical solution to the full governing equation (2.16) at t = 10 which is plotted as a solid black line.

Our model in section 2 used the hydrostatic pressure assumption and for this constant wave solution to be consistent, we require that the shape has a shallow gradient so that:

$$B = \frac{q_0}{UH} \ll 1. \tag{5.15}$$

This is equivalent to requiring that the injection flux is small compared to the natural buoyancy velocity. In contrast to the case of a shock, this condition can be relaxed 12

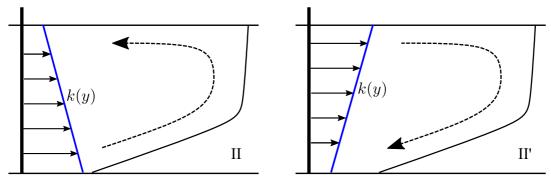


Figure 6: The two different flow structures in a compound rarefaction-shock interface. For parameters in region II ($\Delta k > 0$), the shock is at the base of the shear whilst in region II' ($\Delta k < 0$), the shock is at the top of the shear. The dashed line shows how fluid enters and then exits the nose region in each regime.

when the interface spreads as a rarefaction wave since the gradient becomes progressively shallower at late times.

5.3. Compound rarefaction-shock interface

There are regions of $(\Delta k, M)$ -parameter space outside that given by the inequalities (5.6) and (5.9) in which F(h) is neither concave nor convex. For a linearly varying permeability (equation 3.1), F'(h) has a single maximum, in (0, 1), for those values of M and Δk . The velocity of the interface is then faster in the middle of the aquifer than at the top and the bottom; the buoyant injectate in the middle would then lie underneath the heavy ambient fluid at the top of the aquifer. We assume the vertical adjustment owing to buoyancy and Rayleigh-Taylor fingering is much faster than the along-channel advection of fluid driven by injection (see Huppert *et al.* 2013). In this limit, we expect a compound solution; a rarefaction wave in $h_s < h < 1$ and a vertical shock across $0 < h < h_s$ where h_s is the height of the shock (see figure 2b).

The partial shock travels with a velocity of at least 1 owing to mass conservation. In the region of parameter space outside the full shock region, the velocity of the trailing contact point $M(1 + \frac{\Delta k}{2})$, is less than 1 (see equation 5.9) and hence travels slower than the partial shock. This confirms that when F'(h) has a single maximum in (0, 1), the shock does not occupy the entire depth of the aquifer.

Assuming the partial shock is approximately vertical at late times, mass conservation implies the speed of the shock V, satisfies

$$Vh_{s} = \frac{K(h_{s})}{M + (1 - M)K(h_{s})}$$
(5.16)

which is equivalent to a Rankine-Hugoniot condition. The physical requirement that the interface must be continuous at the contact point between the wave and the shock imposes

$$V = F'(h_s). \tag{5.17}$$

For a linear k(y), equations (5.16) and (5.17) can be solved for V and h_s to give,

$$h_s = 1 - \frac{2}{\Delta k} \pm \sqrt{\frac{2M}{(1-M)\Delta k}}, \quad V = \frac{1}{\left(1-M\right)\left(1 - \frac{2}{\Delta k} \pm 2\sqrt{\frac{2M}{(1-M)\Delta k}}\right)}$$
 (5.18)

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where the positive square root is taken in M < 1, $\Delta k > 0$ (II in figure 4) and the negative in M > 1, $\Delta k < 0$ (II' in figure 4). There are no solutions in the other two quadrants as a compound solution is not possible there. Although II and II' both give rise to compound interface shapes, the flows are physically different, as shown in figure 6. In II, the buoyant injectate migrates along the high permeability region at the base of the aquifer and then rises in the growing nose into the low permeability region, but the interface advances more rapidly in this upper region of the system. In II', $\Delta k < 0$ and the fluid at the top of the aquifer catches the front and is deflected down into the low permeability region.

As with the full shock, we expect the shape of the partial shock not to be a zero-width vertical line because buoyancy smoothes the interface. We adopt a similar approach to that of section 5.2 to find the structure of the partial shock. The shock moves with speed V and to capture its dynamics we seek a travelling wave solution in the shock region $(h < h_s)$. In the rarefaction region $(h > h_s)$, the interface has gradient of order t^{-1} . Assuming we are at long times, we impose the boundary condition $dh/d\eta \to 0$ as $h \to h_s$, on the shape of the shock. We transform the full governing equation (2.16) using the travelling coordinate $\eta = x - Vt$. We drop the time derivative and integrate to find,

$$\frac{\mathrm{d}h}{\mathrm{d}\eta} = \frac{K(h) - Vh(K(h) + M(1 - K(h)))}{MK(h)(1 - K(h))} \quad \text{in } h < h_s, \tag{5.19}$$

where the constant of integration is set to zero to satisfy the condition of zero gradient at $h = h_s$. The matching with the rarefaction region leads to the shape having an infinite horizontal extent in the η coordinates and the position of the leading contact point cannot be determined using mass conservation.

Instead, we solve equation (5.19) numerically with initial condition h(0) = 0 and then translate the solution to fit the full numerical solution at some late time. Figure 5b shows the t = 100 interface as a black line, and the shape given by (5.19) as red dots. In figure 5a, the asymptotic shape is compared to the t = 10 interface. We include the t = 10interface in figure 5b to illustrate that convergence to the full shock shape is much faster than convergence to the partial shock shape. Unlike the full shock shape, the partial shock shape equation (5.19) is only valid in the limit as $t \to \infty$. This is because we imposed that the gradient at $h = h_s$ must be zero but the gradient of the rarefaction is $\mathcal{O}(t^{-1})$ at $h = h_s$.

5.4. Singular solution for $\Delta k = 0$, M = 1

We have found three different late time regimes and the values of the viscosity ratio and permeability difference for which they occur (see figure 4). The four regions I, II, II' and III touch at the point $\Delta k = 0$, M = 1. The late time solutions for this special case of injection of an equal viscosity fluid into a uniform aquifer were found by Huppert & Woods (1995). The distance between the injection well and the fluid-fluid interface is proportional to t and the extent of the front grows proportional to $t^{1/2}$ (see figure 2d), an altogether different result to those found for regions I, II, II' and III. This is a singular solution, since if the aquifer is not uniform or the viscosity ratio is not exactly 1, it is invalid. In that case the late time regime will move to one of the cases described above.

6. Multiple shock solutions

Thus far in this paper we have restricted our attention to aquifers where the permeability increases or decreases linearly from top to bottom. Reservoir rock is typically more complicated than this. Permeabilities can vary significantly over small vertical distances and we expect that there may be more complex late-time regimes as well as the

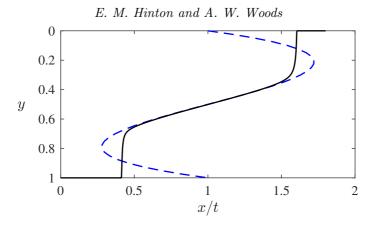


Figure 7: Interface shape for a double-shock (solid black line) at t = 100. The governing equation has been solved numerically for k(y) given by equation (6.1). The blue dashed line illustrates how the permeability varies with height and gives the characteristic speeds F'(h) = k(h) for the advection equation.

three described earlier for the relatively simple linear vertical variations in permeability. It is possible to have two or more separate shocks across the aquifer moving at different speeds. In the analogous problem of viscous channel flow, a double shock has been observed (see Taghavi *et al.* 2009) but not in a porous medium. This can have significant implications for reservoir sweep which is important in both enhanced oil recovery and geologic CO_2 sequestration. In this section, to demonstrate the phenomenon, we consider a more complex cross-layer permeability in which there is a local minimum and local maximum of the permeability within the layer,

$$k(y) = 1 + 15(y - 1)\left(y - \frac{1}{2}\right)y.$$
(6.1)

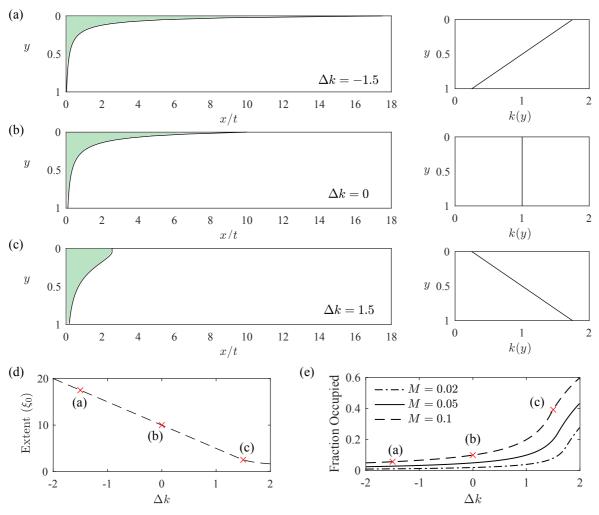
For simplicity, we take M = 1 so that the advection speeds of constant h are given by

$$\frac{\mathrm{d}x}{\mathrm{d}t} = F'(h) = k(h). \tag{6.2}$$

Since there is a local minimum h_{-} and a local maximum h_{+} in the permeability with $h_{-} > h_{+}$, two shock-like regions develop (see figure 7).

7. Implications for CO_2 sequestration

When using geologic formations as a means of storing CO_2 it is important to have accurate estimates of the fraction of the pore space into which CO_2 can be stored. In particular, the critical volume fraction of interest corresponds to the fraction of pore space accessed by the CO_2 between the injection well and the leading contact point of the CO_2 plume (Celia *et al.* 2015). This is because once the leading edge of the plume reaches a particular distance from the injection well, the injection may need to cease, either for reasons of security of storage if there are faults or fractures downstream of the injection well, or in a commercial setting, if different organisations have rights to CO_2 sequestration in adjacent regions of land. The fraction of the pore-space accessed by the CO_2 plume during the injection phase will represent the maximum fraction of the pore-space into which the CO_2 can be sequestered, since the subsequent motion of the CO_2 is controlled by buoyancy, and hence the plume will subsequently tend to thin and



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Figure 8: (a), (b), and (c): Shape of the interface in x/t coordinates for M = 0.1 and three different permeability gradients which are shown in the right-hand column. (d) shows the position of the leading contact point as a function of Δk for M = 0.1. (e) is the fraction of pore space occupied as a function of the permeability gradient for three values of the viscosity ratio typical in carbon sequestration. The red crosses correspond to the interfaces in (a), (b), (c) showing how a steeper interface leads to a greater fraction of pore space invaded.

spread. The impact of the plume structure and shape is therefore key for estimating the efficiency of the sequestration (Bachu 2015).

In this paper we have shown that the presence of a vertical permeability gradient across an aquifer plays a key role in the dynamics of the interface. Here we apply our results to illustrate how such a permeability gradient influences the fraction of pore space accessed by the CO_2 .

We define the available pore space as the product of the position of the leading contact point and the depth of the aquifer. The position of the leading contact point in the $\xi = x/t$ coordinates predicted by the long time asymptotic solutions is a constant, $\xi_0 = x_0(t)/t$.

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Layer depth (H_0)	20m
Porosity (ϕ)	0.15
Density of $CO_2(\rho_i)$	$750 \mathrm{kg}\mathrm{m}^{-3}$
Viscosity of CO ₂ (μ_i)	$4\times 10^{-4} \rm{Pas}$
Viscosity of brine (μ_a)	$4\times 10^{-3} \rm{Pas}$

Table 1: Parameter values for a typical aquifer

The area invaded equals the amount of fluid injected which, in dimensionless variables, is t. The fraction of pore space invaded is the ratio of these two quantities,

$$\frac{t}{x_0(t)} = \frac{1}{\xi_0}.$$
(7.1)

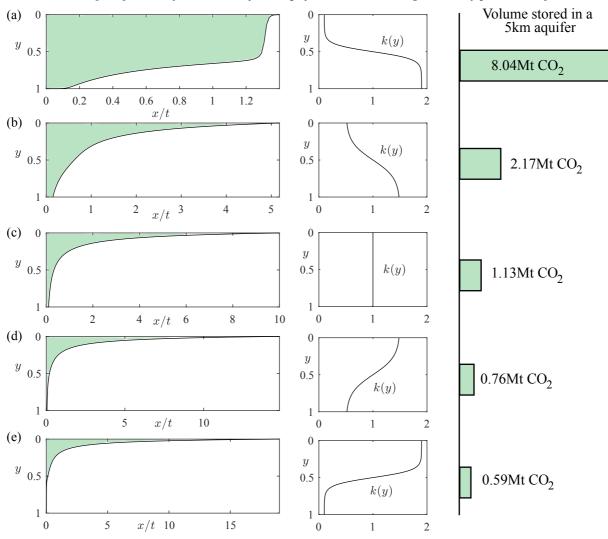
This implies that the fraction of the pore space invaded is independent of time, as found by Guo *et al.* (2016b) for a radial, vertically homogeneous aquifer. Unlike the radial case however, the fraction invaded is independent of the buoyancy parameter (2.17) because at late times the role of buoyancy can be neglected.

Supercritical carbon dioxide is typically much less viscous than the ambient brine in storage sites and we take the values M = 0.1, 0.05, and 0.02 in our examples since M varies with the depth of the aquifer. In the classical model with $\Delta k = 0$, these choices of M lead to the interface following the shape of a rarefaction wave with the injectate migrating fastest at the top of the aquifer. For $\Delta k < 0$, the CO₂ migrates even faster at the top of the aquifer of pore space invaded is reduced. Conversely for $\Delta k > 0$, the interface is steeper and the pore space occupied is greater. The interfaces for these three cases are shown in figure 8 for M = 0.1 and $\Delta k = 0, \pm 1.5$. The right-hand column of figure 8 shows the associated permeability profiles. For sufficiently large Δk , the parameters move from region I into region II in figure 8 c). The fraction occupied for each of our parameter choices is labelled (a), (b), and (c) in figure 8 which illustrates how the fraction of pore space occupied on Δk for our three choices of M.

It is clear that the fraction of pore space invaded is highly dependent on the permeability profile; for example, when M = 0.1, in an aquifer with $\Delta k = 1.5$ the CO₂ invades approximately four times the pore space invaded in a uniform aquifer of the same mean permeability. For reference, $\Delta k = 1.5$ represents an aquifer in which the permeability varies by a factor of 7. Using the Kozeny-Carman relation that suggests the permeability is proportional to the grain size squared, $\Delta k = 1.5$ only requires the grain size to vary by a factor of 2.65 accross the aquifer which is within measured values for many aquifers (Carman 1939). Therefore, in making storage estimates there is an important uncertainty associated with vertical heterogeneities. Our results could be applied to find the probability distribution of the fraction of pore space occupied given a large data set of permeability variations in aquifers.

7.1. CO_2 storage in a real aquifer with lenses of high and low permeability

In this subsection, we extend the analysis above to the case of a nonlinear permeability profile and we calculate how the permeability structure influences the volume of CO_2 stored in a typical project. We compare permeability profiles, each with the same mean permeability, in which there are lenses of high and low permeability. These profiles are



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Figure 9: Interface shapes and volume of CO_2 stored for nonlinear permeability profiles including lenses of high and low permeability. The first column shows the interface shape in x/t coordinates, and the corresponding permeability profile is shown in the second column. We calculate the volume of CO_2 stored for each permeability profile in an aquifer which is 20m deep and 1000m wide, assuming injection must stop when the leading edge of the plume has travelled 5000m from the injection well. The paramter values are given in table 1. The location of the high and low permeability lenses has a significant influence on the volume stored.

shown in figure 9, and the left-hand column shows the interface shape. We assume the aquifer and the injection well are one kilometre wide (in the direction out of the plane in figure 9). We can calculate the mass of CO_2 stored using the parameter values in table 1. We assume injection is required to stop when the plume reaches a point five kilometres from the injection well. These volumes are shown in figure 9 and demonstrate

that the volume of CO_2 stored is heavily dependent on the location of the low and high permeability lenses.

8. Conclusion

In this contribution we have analysed the injection of buoyant fluid into an aquifer where the permeability varies vertically. With a permeability that varies linearly with height, we have found four late time regimes including a compound rarefaction-shock interface which does not occur in a uniform porous medium. Our parameter space shows that the classic solution for equally viscous fluids in a uniform aquifer is singular and unstable to small changes in the permeability profile. Applying our results to the problem of carbon storage, we have shown that cross-aquifer permeability differences can significantly influence the volume of CO_2 that can be stored in an aquifer. When the assumption of permeability that varies only linearly with height is relaxed, we have found that it is possible to have two separate shocks that travel at different speeds in a porous medium. Our study has shown that the early time period is dependent not only on the viscosity ratio but also on the permeability at the top of the aquifer.

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REFERENCES

- BACHU, STEFAN 2015 Review of CO2 storage efficiency in deep saline aquifers. International Journal of Greenhouse Gas Control 40, 188–202.
- BARENBLATT, G. I. 1952 On some unsteady motions of fluids and gases in a porous medium. *Prikl. Mat. Mekh.* 16, 67–78.
- BEAR, JACOB 1971 Dynamics of flow in porous media. Elsevier.
- BJORLYKKE, KNUT 1993 Fluid flow in sedimentary basins. Sedimentary Geology 86 (1-2), 137–158.
- CARMAN, P. C. 1939 Permeability of saturated sands, soils and clays. The Journal of Agricultural Science 29, 262.
- CELIA, M. A., BACHU, S., NORDBOTTEN, J. M. & BANDILLA, K. W. 2015 Status of CO2 storage in deep saline aquifers with emphasis on modeling approaches and practical simulations. *Water Resources Research* **51** (9), 6846–6892.
- FARCAS, ADRIAN & WOODS, ANDREW W 2016 Buoyancy-driven dispersion in a layered porous rock. J. Fluid Mech 767, 226–239.
- FAYERS, F.J., BLUNT, M.J. & CHRISTIE, M.A. 1992 Comparisons of Empirical Viscous-Fingering Models and Their Calibration for Heterogeneous Problems. Society of Petroleum Engineers.
- GOLDING, MADELEINE J., NEUFELD, JEROME A., HESSE, MARC A. & HUPPERT, HERBERT E. 2011 Two-phase gravity currents in porous media. *Journal of Fluid Mechanics* 678, 248– 270.
- GUNN, IAIN & WOODS, ANDREW W 2011 On the flow of buoyant fluid injected into a confined, inclined aquifer. J. Fluid Mech 672, 109–129.
- GUO, BO, BANDILLA, K.W., NORDBOTTTEN, J.M., KEILEGAVLEN, E. & DOSTER, F. 2016a A multiscale multilayer vertically integrated model with vertical dynamic for CO2 sequestration in layered geological formations. Water Resources Research 52, 6490–6505.
- GUO, BO, ZHENG, ZHONG, BANDILLA, KARL W., CELIA, MICHAEL A. & STONE, HOWARD A. 2016b Flow regime analysis for geologic CO2 sequestration and other subsurface fluid injections. International Journal of Greenhouse Gas Control 53, 284–291.

Buoyancy-driven flow in a confined aquifer with a vertical gradient of permeability 19

- HESSE, M, TCHELEPI, H A & ORR, FRANKLIN M 2006 Scaling Analysis of the Migration of CO2 in Saline Aquifers. Society of Petroleum Engineers .
- HESSE, M. A., TCHELEPI, H. A., CANTWEL, B. J. & ORR, F. M. 2007 Gravity currents in horizontal porous layers: transition from early to late self-similarity. *Journal of Fluid Mechanics* 577, 363.
- HESSE, M A & WOODS, A W 2010 Buoyant dispersal of CO2 during geological storage. *Geophys. Res. Lett* **37**.
- HUPPERT & WOODS 1995 Gravity-driven flows in porous layers. J. Fluid Mech 292, 55-69.
- HUPPERT, HERBERT E & NEUFELD, JEROME A 2014 The Fluid Mechanics of Carbon Dioxide Sequestration. Annual Review of Fluid Mechanics 46 (1), 255–272.
- HUPPERT, HERBERT E., NEUFELD, JEROME A. & STRANDKVIST, CHARLOTTE 2013 The competition between gravity and flow focusing in two-layered porous media. *Journal of Fluid Mechanics* **720**, 5–14.
- JUANES, RUBEN, MACMINN, CHRISTOPHER W. & SZULCZEWSKI, MICHAEL L. 2010 The footprint of the CO2 plume during carbon dioxide storage in saline aquifers: Storage efficiency for capillary trapping at the basin scale. *Transport in Porous Media* 82 (1), 19–30.
- KURGANOV, ALEXANDER & TADMOR, EITAN 2000 New High-Resolution Central Schemes for Nonlinear Conservation Laws and ConvectionDiffusion Equations. *Journal of Computational Physics* 160 (1), 241–282.
- LAJEUNESSE, E, MARTIN, J, RAKOTOMALALA, N, SALIN, D & YORTSOS, Y C 1999 Miscible displacement in a Hele-Shaw cell at High Rates **398**, 299–319.
- LAKE, LARRY W. 1989 Enhanced Oil Recovery. Prentice Hall.
- LYU, XIAOYING & WOODS, ANDREW W. 2016 Experimental insights on the development of buoyant plumes injected into a porous media. *Geophysical Research Letters* **43** (2), 709– 718.
- MACMINN, CHRISTOPHER W. & JUANES, RUBEN 2009 Post-injection spreading and trapping of CO2 in saline aquifers: Impact of the plume shape at the end of injection. *Computational Geosciences* **13** (4), 483–491.
- MACMINN, CHRISTOPHER W., NEUFELD, JEROME A., HESSE, MARC A. & HUPPERT, HER-BERT E. 2012 Spreading and convective dissolution of carbon dioxide in vertically confined, horizontal aquifers. *Water Resources Research* **48** (11), 1–11.
- PEGLER, SAMUEL S., HUPPERT, HERBERT E. & NEUFELD, JEROME A. 2014 Fluid injection into a confined porous layer. J. Fluid Mech. 745, 592–620.
- PRITCHARD, D., WOODS, A. W. & HOGG, A. J. 2001 On the slow draining of a gravity current moving through a layered permeable medium. J. Fluid Mech. 444, 23–47.
- PRUESS, KARSTEN, GARCÍA, JULIO, KOVSCEK, TONY, OLDENBURG, CURT, RUTQVIST, JONNY, STEEFEL, CARL & XU, TIANFU 2004 Code intercomparison builds confidence in numerical simulation models for geologic disposal of CO2. *Energy* **29** (9-10), 1431–1444.
- RIAZ, A., HESSE, M., TCHELEPI, H. A. & ORR, F. M. 2006 Onset of convection in a gravitationally unstable diffusive boundary layer in porous media. *Journal of Fluid Mechanics* 548, 87111.
- TAGHAVI, S. M., SEON, T., MARTINEZ, D. M. & FRIGAARD, I. A. 2009 Buoyancy-dominated displacement flows in near-horizontal channels: the viscous limit. *Journal of Fluid Mechanics* 639, 1–35.
- WOODS, ANDREW W. 2014 Flow in Porous Rocks: Energy and Environmental Applications. Cambridge University Press.
- WOODS, ANDREW W. & FARCAS, ADRIAN 2009 Capillary entry pressure and the leakage of gravity currents through a sloping layered permeable rock. *Journal of Fluid Mechanics* **618**, 361.
- ZHENG, ZHONG, GUO, BO, CHRISTOV, IVAN C, CELIA, MICHAEL A & STONE, HOWARD A 2015 Flow regimes for fluid injection into a confined porous medium. J. Fluid Mech 767 (2015), 881–909.